

# UNIVERSIDAD DE INVESTIGACIÓN DE TECNOLOGÍA EXPERIMENTAL YACHAY

## Escuela de Ciencias Químicas e Ingeniería

## TÍTULO: REINFORCEMENT OF RECYCLED PET: A REVIEW

Trabajo de integración curricular presentado como requisito para la obtención del título de Petroquímico

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## DEDICATORIA

Por su apoyo incondicional, A Dios, A mis padres Edward Guzmán y María Cajamarca, A mis hermanos Roser, Ariel y Alejandra

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#### RESUMEN

En el siguiente trabajo de investigación se hizo una revisión bibliográfica de las estrategias empleadas para mejorar las propiedades del PET reciclado. El tipo de reciclado en el cual se profundizó fue el análisis secundario por la cantidad de información encontrada al respecto. Para llevar a cabo la presente investigación se revisaron los artículos de los últimos cinco años en los que se utilizaron el PET reciclado como matriz polimérica los cuales fueron revisados, analizados y clasificados en cuatro secciones: PET reciclado, mezclas con PET reciclado, extendedores de cadena y nano-partículas de relleno. Los valores obtenidos fueron resumidos en tablas para el análisis de sus tendencias, diferenciando las propiedades mecánicas y térmicas. Para explicar el comportamiento de las mezclas se utilizaron los datos reportados en DSC, TGA, SEM y ensayos mecánicos. Los resultados mostraron dos tendencias principales en las mezclas: la primera enfocada en el endurecimiento de la mezcla usando una fase dispersa con un módulo de Young mayor al de la matriz o utilizar un polímero con una rigidez menor a la matriz pero que debido a mecanismos de endurecimiento incrementa sus propiedades mecánicas; la segunda tendencia se centra en la utilización de polímeros que generan propiedades plastificantes.

**Palabras clave:** Estrategias para el reciclado del PET, extendedores de cadena, nanopartículas de relleno, mezclas con PET reciclado

#### ABSTRACT

A bibliographic review was made about strategies used to improve the thermal and mechanical properties of recycled PET in the following work. To carry out this research, articles in which recycled PET was used as a polymeric matrix from the last five years were reviewed, analyzed, and classified into four sections: recycled PET, blendings with recycled PET, chain extenders, and filler nanoparticles. Values obtained were summarized in tables for the analysis of their trends, differentiating mechanical and thermal properties. The data obtained by DSC, TGA, SEM, and Tensile tests were used to explain the behavior of the blends. Results showed two main tendencies in the blends: the first focused on the hardening PET using a dispersed phase with Young's modulus greater than polymeric matrix. The second trend focuses on the use of polymers that generate plasticizing properties in the blend.

**Keywords**: PET recycling strategies, chain extenders, filler nanoparticles, blends with recycled PET

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## LIST OF ABBREVIATIONS

American Society for Testing and Materials	ASTM
Ammonium polyphosphate	APP
Bis hydroxy ethylene terephthalate	BET
Differential Scanning Calorimeter	DSC
Dimethyl terephthalate	DMT
Ethylene glycol	EG
Fourier transform infrared spectroscopy	FTIR
International Organization for Standardization	ISO
Maleic anhydride	PP-g-MA
Melt Flow Index	MFI
Montmorillonite	MMT
Poly(butylene adipate-co-terephthalate)	PBAT
Poly(butylene terephthalate)	PBT
Poly(ethylene 2,6-naphtalate)	PEN
Poly(ethylene terephthalate)	PET
Poly(ethylene)	PE
Polycarbonate	PC
Polypropylene	PP
Recycled poly(ethylene terephthalate)	R-PET
Scanning electron microscope	SEM
Styrene-ethylene-butadyene-styrene copolymer	SEBS
Terephthalic acids	ТА
Thermogravimetric analysis	TGA
Virgin poly(ethylene terephthalate)	V-PET

## CHAPTER I INTRODUCTION

#### 1.1. Introduction

The use of synthetic polymers in the food industry allows extending the life cycle of aliments, representing an energetic saving and money saving<sup>1</sup>. However, the fast residues generation becomes an environmental problem due to the accumulation of these in the terrestrial layer <sup>2–4</sup>.

Poly(ethylene terephthalate) (PET) is one of the most widely used thermoplastics due to its relatively low production costs, recyclability, mechanical attractiveness, barrier properties, moisture resistance, and low permeability to gases such as oxygen and carbon dioxide <sup>2</sup>,<sup>5</sup>. That is why this material is industrial and economically attractive; its production has increased exponentially from 13 million tons in the '90s to 16 million in 2013 <sup>6</sup>. The global production of PET in 2018 exceeded 20.1 million tons with an increase of 5.2% annually between 2012 and 2017<sup>6</sup>, and average annual growth of 6.9% is expected between 2017-2025<sup>2</sup>. Its production is destined between 83-84% to the packaging of beverages and soft drinks worldwide<sup>6</sup>.

PET is a polymer that does not create a high quantity of contaminants during its production or degradation. The increase in plastic waste and its high resistance to biological and atmospheric agents can be considered a polluting material because of its accumulation <sup>7</sup>.

The high demand for PET worldwide and its resistance to biological agents have made researchers focus on recycling PET as the primary option for its final use. The recycling of a material is a strategy to: i) reduce the emission of gases during the manufacture, transport, and disposal of solid waste and ii) conserve non-renewable natural sources <sup>2</sup>. The implementation of this strategy is essential because, in addition to those mentioned above, it helps to save energy, lower fuel consumption, reducing landfills, and reduction of greenhouse gases <sup>8</sup>. Recycling one ton of PET saves the emission of 1.5 tons of carbon

dioxide, representing a saving of 70% compared to V-PET in the manufacture of plastic bottles<sup>9</sup>.

According to the Guidelines for the recovery and recycling of plastics waste, established by the International Organization for Standardization (ISO) <sup>10</sup> and the Standard Guide for Waste Reduction published by the American Society for Testing and Materials (ASTM), 4-four main processes have been established for the recycling of materials:

- **Primary recycling.** It is about reusing flakes of PET-based materials that were produced during the shaping of the product.

- **Mechanical recycling.** During this process, the main structure of the material is preserved, and many of its potentials can be used in similar applications by replacing the virgin material <sup>11</sup>. Low investment is required for this and the use of affordable equipment and the low adverse environmental impact <sup>5</sup>. This process consists of several stages such as separation, washing, and milling of waste containers.

- **Chemical recycling.** It includes the depolymerization of waste materials to restore (recover) monomers that can be re-polymerized. This route requires a significant capital investment, high energy costs, and needs large scales to be economically viable<sup>5</sup>. This process can be carried out in several types: methanolysis, glycolysis, and hydrolysis.

- Quaternary recycling. It leads to getting energy from the incineration of polymer wastes.

Despite the advantages mentioned above regarding recycling, several obstacles arise when carrying out recycling processes, such as the high cost of collection and separation, the presence of colored debris, and oxidative degradation products that cause yellowing compromising mechanical properties of PET. The recycling of PET supposes a deterioration of its physical-mechanical properties due to the reduction of its molar mass, viscosity, and melting point <sup>12</sup>.

According to recent studies, the properties of R-PET are modified by the reactive extrusion through chain extenders, copolymers, and some additives. Despite the extensive use of mechanical R-PET, with various applications such as reinforcement in cementitious matrices, coatings, insulating materials, bottles for beverage, its use is limited due to the detrimental effect of the recycling process on its properties. That is why the need to use external (addition of) compounds that allow modifying PET properties so that its use is massified as its similar V-PET <sup>5</sup>.

Immiscibility of polymers, such as PET, during the blending, can be improved by adding copolymers, particularly block and graft copolymers, with segments capable of undergoing specific interactions through chemical reactions with the constituents of the blend, or by mixing suitable functionalized polymers promoting improved interactions. These copolymers, which are called compatibilizers, can be added or formed in situ during fusion by fusion through the interfacial chemical reaction of the polymer components <sup>13</sup>.

On the other hand, the addition of well-dispersed nanoparticles in a polymer matrix favors polymer reinforcements, changing the mechanical behavior, the barrier properties, the thermal and rheological properties, which depend on the degree of dispersion and amount of the added additive <sup>14</sup>.

Among the different processes involved in material recycling, primary recycling would seem to be the best treatment when the waste material to be recycled has been very little contaminated. However, this requirement of high purity, cleanliness, and homogeneity of the material could result in a disadvantage. That is why it seeks to take advantage of mechanical recycling, the second-best from an environmental point of view produces fewer greenhouse gases than its two subsequent processes <sup>15</sup>

1.2. Problem Statement

R-PET properties are less attractive than virgin material; that is why many researchers work on an economically feasible solution to this problem. To date, there is no compilation of these efforts in the recent literature. The present review surge as a response to the necessity of the researchers to have updated results on this matter, and a comparative analysis, that will help to establish a state of the art in the strategies employed to improve the mechanical and thermal properties of R-PET.

In the present review, an analysis of the strategies used to improve the properties of R-PET is developed to analyze its mechanical and thermal properties. Based on the information collected (reviewed), propose the best options to be implemented to carry out the recycling process of PET.

#### 1.3. Objectives

- 1.3.1. General Objective
- To review the literature published since 2015 about the reinforcements used in R-PET matrices.
- 1.3.2. Specific objectives
- Identify in the literature how thermal and mechanical properties of reinforcements with R-PET are modified.
- To review the most used strategies in the reinforcement of R-PET.
- Identify in the literature what are the problems associated with polymer blends and analyze their reinforcing effect.

# CHAPTER II THEORETICAL FRAMEWORK

#### 2.1. Recycling of PET

PET is the third most widely used thermoplastic in the world <sup>16</sup>, <sup>17</sup>. This semicrystalline thermoplastic can be found in films, sheets, strapping, packaging, and fibers used for sacking. The recycling of PET is inferior visually, physically, and chemically; that is why recycle companies intend to join efforts to obtain a recycled material as close to V-PET <sup>18</sup>. Once V-PET is used, the recycling process begins and is carried out into 4-main processes that will be developed in detail in the present chapter.

*Figure 1* shows the polymerization, formulation, and processing stages to convert crude oil to final products. Once consumed, the plastic is discarded by the consumer and turned into waste taken to first recycling; This recycled material is introduced into the main processing production line. The new waste produced is taken to secondary recycling and introduced into the Formulation and Compounding line. After tertiary recycling, the waste is taken to the Quaternary recycling where this material is converted into energy in the form of heat<sup>19</sup>.



Figure 1. The life cycle of plastics<sup>19</sup> (Adapted from R. Clift)

These stages allow optimal use of the plastics for their recovery, which will be discussed in the next section.

2.1.1. Primary recycling

Primary recycling is about the reintroduction of processing waste into the extrusion cycle to produce the same products. These residues can be edges or scrap. This type of recycling is the best recycling method because it uses less energy and fewer resources than the following three recycling processes<sup>15</sup>,<sup>20</sup>.

These wastes must be carried out for some process: collection and identification, selection and separation of cleanest materials from those with additives, grinding and homogenization of the wastes to be extruded, washing with hot water finally, the material is extruded to be processed once again <sup>15</sup>.

2.1.2. Secondary recycling

This process is also known as mechanical recycling. It is about recovering solid plastic waste through mechanical processes to obtain sufficient properties instead of V-PET <sup>15</sup>. To carry out secondary recycling is necessary to follow some steps<sup>1821</sup>: separation and classification of wastes depending the shape, density, size, and color; washing and drying to eliminate organic compounds, grinding of the material to homogenize it and make easier its mobilization and extrusion, and finally composite and granulation of the flakes of R-PET with other components for posterior extrusion.

This process eventually degrades the polymer partially and, therefore, deteriorates the properties of its V-PET predecessor. In order to improve the properties of the material, it is necessary to use new components that complement the R-PET, forming blends of V-PET with other compounds. Currently, different components are used, such as virgin polymer, fillers, fibers, or compatibilizers<sup>18,5,13</sup>.

2.1.3. Tertiary recycling

Tertiary recycling or commonly known in the industry as chemical recycling. It consists of a chemical transformation of polymer chains into monomers or smaller molecules that can be used as raw materials to produce new polymers for the same or new applications<sup>15</sup>,<sup>5</sup>. This process has several reaction pathways, as presented in *Figure 2*,this

scheme shows four main reactions by which chemical recycling can occur, depending on the reaction medium. <sup>22</sup>,<sup>17</sup>,<sup>21</sup>



Figure 2. Reaction pathways of chemical recycling (Adapted from Thiounn et al.<sup>22</sup>)

#### 2.1.3.1. Hydrolisis

It is a depolymerization process in which intervenes large water-PET ratios (5:1) at elevated temperatures and/or in the presence of catalysts. The main products obtained in this process are terephthalic acids (TA) and Ethylene glycol (EG)<sup>22</sup>. It can be carried out by acid hydrolysis, alkaline hydrolysis or neutral hydrolysis.

#### 2.1.3.2. Methanolysis

Methanolysis is based on the treatment of PET with methanol at temperatures between 180 and 280 °C and pressures between 20-40 atm in the presence of a catalyst, zinc acetate is commonly used. This reaction gives as main products dimethyl terephthalate (DMT) and ethylene glycol (EG).<sup>21</sup>,<sup>22</sup>

#### 2.1.3.3. Aminolysis

Aminolysis is a reaction that uses amines for the depolymerization of PET. This process has not been widely studied due to the costs of amine and its toxicity. This reaction yields TA diamides as main products<sup>22</sup>,<sup>23</sup>.

2.1.3.4. Glycolysis

Glycolysis is the simplest and oldest method for the depolymerization of PET <sup>21</sup>,<sup>22</sup>. This process is carried out in a batch reactor, obtaining as main product bis hydroxy ethylene terephthalate (BET) <sup>17</sup>,<sup>24</sup>. Glycol diffuses into the polymer to react with an ester and breaks down PET into smaller fractions <sup>21</sup>. The catalysts that are normally used to increase glycol activity and decrease reaction time are methyl acetate, titanium phosphate, and ferrous oxide. <sup>24</sup> This recycling method is the most used due to the various applications of the products obtained. <sup>21</sup>,<sup>17</sup>,<sup>24</sup>

2.1.4. Quaternary Recycling

Quaternary recycling consists of the incineration of plastic for energy recovery through the production of heat. Currently, this type of recycling is widely used due to its ease of using<sup>15</sup>. In the European Union, 39.5% of plastic waste is still recovered through this process<sup>25</sup>. This process is used when mechanical processes fail due to contamination excess<sup>15</sup>

2.2. New Techniques for Recycling

In recent years, new recycling techniques have been developed to improve the reaction and purity of polyesters in chemical and mechanical processes, respectively.

2.2.1. DEMETO technique

This patent was developed in 2013 by Gr3n company, and it improves the depolymerization performance of polyesters with additives such as pigments and textiles. The process is known as depolymerization by microwave technology, and it is capable of reducing the time of reaction to 10 minutes<sup>26</sup>.

#### 2.2.2. Chemical wash

In mechanical recycling, one more step is added to improve the purity of the recycled material. An additional step could be implemented in industrial processes after conventional washing and before the drying stage. This wash consists of removing the Surface layer of the PET material, with sodium hydroxide, with the proposal of forming a new cleaner surface than the original one. This process allows obtaining PET with fewer contaminants and greater added value.<sup>18</sup>

#### 2.3. Degradation of PET

As it is already known, Mechanical recycling is about eliminating impurities by sorting, grinding, washing, and extruding (at a controlled temperature). One of the drawbacks of mechanical recycling is thermo-mechanical and hydrolytic degradation, which decreases molecular weight. Eventually, its viscosity, melt strength, mechanical properties, and so on limit its usefulness for many applications <sup>3,6,27–30</sup>. This degradation makes mechanical recycling a finite process due to its constant degradation<sup>27</sup>.

*Figure 3* shows the scission reactions that PET undergoes during extrusion corresponding to thermal and hydrolytic degradation, respectively. In *Figure 3a*, the thermal decomposition of an ester linkage is shown, caused by an increase in temperature during the extrusion process resulting in carboxylic acid end groups and vinyl ester end groups. In *Figure 3b* it is shown the hydrolysis reaction of PET is caused by the presence of water that gives; as a result, carboxylic acid end groups and hydroxyl-ester end groups. Increasing carboxyl groups result in a decrease in molecular weight <sup>27</sup>.

Thermal degradation	Hydrolytic degradation
PET polymer	PET polymer
- С- он + сн <sub>а</sub> =сно-с-С-	

Figure 3. Effect of processing on the chain scission reactions of PET ester linkages (Adapted from Asensio et al. <sup>27</sup>)

## CHAPTER III

## RECYCLED PET: GENERAL PROPERTIES, BLENDS, AND ADDITIVES

#### 3.1. Recycled PET properties

Mechanical and thermal properties of PET deteriorate with the recycling process, in contrast with V-PET. It is due to degradation, pollutants, recycling mechanisms, among others. During the recycling process occurs a cleavage of chains, an increase of carboxylic groups, a reduction in molecular weight, and so on a decrease in intrinsic viscosity, resulting in a deterioration of the mechanical and thermal properties of R-PET. Such is the case reported by Lee et al.<sup>31</sup>, who studied properties of R-PET, V-PET and blends at different sample compositions. *Figure 4* shows thermogravimetric analysis results where can be compared thermal degradation of R-PET and V-PET in function of the temperature increase. It can be seen that for 2 and 5 wt% V-PET experienced a high resistance to weight loss related to cleavage of chains during recycling process of PET.



Figure 4. Thermal degradation of weight loss of 2 wt% and 5 wt% It c

According to Oromiehie et al., <sup>29</sup> samples of R-PET go down their intrinsic viscosity. *Figure 5* shows the composition of several R-PET/V-PET samples with several compositions and intrinsic viscosity according to the extrusion technique applied. Like it can be seen, all the samples tend to decrease their intrinsic viscosity, and this trend is associated with the amount of R-PET used.



*Figure 5.* Intrinsic viscosity of several samples with virgin and recycled PET (Recovered from Oromiehie et al.<sup>29</sup>)

This trend is because of the thermal exposure as well as shear degradation of R-PET. As a direct result, it produces a plastic material with a reduced melt viscosity, which means molecular weight decreases while the amount of R-PET increases. One of the reasons for this phenomenon is the retained humidity from the specific surface of the wastes. In consequence, traces of humidity promote chain scission with a low intrinsic viscosity <sup>29</sup>, <sup>32</sup>, <sup>33</sup>.

The mechanical properties and the standards employed for testing the samples of neat R-PET, are compiled in Table 1. Even though several samples were tested under the same international standards, considerably different values were obtained depending on the sources of R-PET employed by the authors. Such is the case of Srithep et al. <sup>34</sup>, who reported tensile strength of 60 MPa compared to Thumsorn et al. <sup>3</sup>, who obtained a tensile strength of  $10 \pm 5$  MPa. This may be due to several factors such as i) the source of obtaining the PET, ii) the post-collection treatment of the PET, iii) the extrusion process that can take place in a single crew, co-rotating or counter-rotating (twin-screw extruder)<sup>32,35</sup>.

Matrix	Additive	Composition matrix/additive	Property	ISO/ASTM	Test method	Value (unit)	Reference	
			1	Tensile strength	ASTM D-638 at cross-head	Tensile	60 MPa	34
			Tensile modulus	speed of 20 mm/min	testing	2.8 GPa	34	
				Flexural strength	ASTM D-790 with span length of 48mm and testing speed of	Flexural	70 MPa	34
			Flexural modulus	3mm/min	test	2.3 GPa	34	
			Tensile strength			$10 \pm 5$ MPa	3	
		e 100/0	Elongation	ASTM-D-638-02	Tensile	2.5 %	3	
			Tensile Modulus		testing	$1500\pm50~\mathrm{MPa}$	3	
			Tensile strength			460 ± 94 MPa	36	
R-PET	None		/0 strain at break ASTM D 638	Tensile testing	49.2 ± 1.05 MPa	36		
			Tensile modulus			5451± 69 MPa	36	
			Impact resistance		Tensile	8.1 KJ/ $m^2$	37	
			Toughness	ASIM D638-10	testing	12.8 $MJ/m^3$	37	
			Tenside modulus		Tensile testing	3461 ± 81.8 MPa	38	
			strain at break	ISO 527 standard 10kN at 50 mm/min		$1.8 \pm 0.1$ %	38	
			Tensile strength			40 ±3.3 MPa	38	

Table 1. Mechanical properties of representative R-PET without additives

	Tensile strength	ASTM D638-10 crosshead speed of 5 mm/min	Tensile testing	35 ± 3 Mpa	39
	Tensile modulus			600.3 ± 19.1 MPa	40
	Tensile strength	ISO 527-1:2012	Tensile testing	$56.8\pm0.8~\mathrm{MPa}$	40
	Elongation at break			$494.6 \pm 9.7$ %	40
	Charpy Impact strength	ISO 179-1:2010	Charpy Impact	$2.87 \pm 0.42 \text{ KJ}/m^2$	40

In all cases, a decrease of intrinsic viscosity is reported, such as the data reported by Oromiehie et al.<sup>29</sup>, who dated a decrease of intrinsic viscosity of 23.81%. This decrease is related with molecular weight as shown in the next formula <sup>41</sup>

$$n_{sp,i} = K_m C_i M_i^a$$

Where  $K_m$  is the Mark-Houwink-Sakurada coefficient, *a* is a variable usually in the range between 0.5-1,  $C_i$  and  $M_i$  are the concentration and the molecular weight, respectively, of i the component. As it can be seen, molecular weight affects directly proportional intrinsic viscosity of a blend. It means if molecular weight decreases, then intrinsic viscosity will as well. This decrease allows the presence of carboxylic acids, and in such a way, a greater cleavage of PET chains can occur. According to Oromiehie et al.<sup>29</sup>, this cleavage decreases the molecular weight in a 30.61% contrasting molecular weight of V-PET with R-PET. This fact eventually promoted a decrease in mechanical properties such as Tensile Modulus and Flexural strength, as shown in *Table 1*.

On the other hand, the degree of crystallinity varies depending on several factors like chain entanglements and branching. Such is the case of Kiliç et al.<sup>42</sup>, who used R-PET flakes provided by SASA Plyester San. A.Ş., Company of Turkey as matrix for being blended with organoclay nanocomposite fibres in order to analyze morphological, thermal, surface and mechanical properties. They reported a crystallinity value for R-PET of 3.53%. This value is contrary to the exposure by Torres et al.<sup>35</sup> who used post-consumer PET bottles and V-PET resins to study the thermal an mechanical properties of V-PET and R-PET. They reported a loss of crystallinity of 33% (from 46% to 31%) which was related with the structure of V-PET (isotropic character) versus R-PET (Anisotropic character). Han et al.<sup>43</sup> studied and characterized V-PET and R-PET fibers. They reported an increase in crystallinity of 59.84% (from 26.57% to 42.47%) which was related with high mechanical properties such PC, PEN, among others. *Table 2* presents thermal values of R-PET with no presence of additives, recovered from different researches at different test conditions.

		Composition						
Matrix	Additive	matrix/additive	Property	ISO/ASTM	Test method	Value (unit)	Reference	
			Thermal degradation 5%		Thermal	399.3 °С	34	
					Thermal degradation 50% None Descomposition	None	degradation	436.8 °C
			energy		temperature	262.2 KJ/mol	34	
			Glass transition temperature	Specimens of 4 to 5 mg were		81.5 °C	3	
			Melting point	placed in aluminium sample	DSC	245.9 °C	3	
			Melting Enthalpy	pans and heated from $-10^{\circ}$ C to 280°C at a 10 °C/min	220	41.2 J/g	3	
			Cristalinity degree	200 0 at a 10 0/1111		34.3 %	3	
			Thermal degradation 10%			409.1 °C	3	
R-PET None	100/0	Thermal degradation 20%	<b>N</b> T	Thermal	425.2 °C	3		
	None	None 100/0	Thermal degradation 10%	None	degradation temperature	420 °C	44	
			Thermal degradation 20%			429 °C	44	
			Glass transition temperature	Heating from 25 °C to 300 °C at a rate of 5 °C/min	DSC	68.43 °C	37	
			Melting point			256.03 °C	37	
			cristalization temperature			117.89 °C	37	
			Melting Enthalpy			47.74 J/g	37	
			Cristalinity degree			100.47 %	37	
			Melt flow index	ASTM D1238	MFI	89.3 ±12.3 mm/10min	38	

#### Table 2. Thermal properties of representative R-PET without additives

Crystallization temperature			204 °C	38
Glass transition temperature	Samples heated from 30 °C to	Dec	78.9 °C	38
Melting point	300 °C at a rate of 10 °C/min under nitrogen atmosphere	DSC	251 °C	38
Melting Enthalpy	under mit ogen unnosphere		36.6 J/g	38
Cristalinity degree			30.5 %	38
Onset temperature			432 °C	38
Thermal degradation 50%	None	TGA	453 °C	38
Endset temperature			470 °C	38
Glass transition temperature			73 °C	39
Melting point	samples were heated from 25°C to 300°C with a heating	DSC	250.7 °C	39
Melting Enthalpy	rate of 10°C/min	DBC	35.2 J/g	39
Cristalinity degree			26.1 %	39
Glass transition temperature	sample was nearly 5 mg and the thermal cycle for the		75.7 °C	13
temperature	determination of the	DSC	127.7 °C	13
Melting point	ramp from 20 until 280 °C with		250.7 °C	13
Melting Enthalpy	10 °C/min heating rate.		55.4 J/g	13
Glass transition temperature			82.0 ±0.7 °C	40
Cold crystallization temperature	heated from 30 to 280 °C with	DSC	150 8+ 0 4 °C	40
Melting point	a speed of 10 °C /min		$244.9 \pm 0.9 \ ^{\circ}\text{C}$	40
Crystallinity degree			$10.6 \pm 0.5$ %	40
Thermal degradation 5% (air)		TGA	$405.4 \pm 0.2 \ ^{\circ}\text{C}$	40

Residual mass at 700 °C	5-7 mg heated from 30-700 °C. Speed 20 °C /min		1 26 + 0 04 %	40
Glass transition temperature	Speed 20°C / min		79.94 °C	42
Crystallization temperature	Samples in a nitrogen atmosphere heated from 20 to	DSC	212.33 °С	42
Melting point	350 °C with a speed of 10 °C	DBC	241.21 °C	42
Melting Enthalpy	/min		28.11 KJ/kg	42
Crystallinity degree			3.53%	42
Decomposition temperature	samples heated up to 900 °C		375.35 °C	42
(N2)	under $N_2$ flow with a speed of 10 °C /min	TGA	311.39 °C	42
(N2)			355.34 °C	42
Melting point	Analysed under nitrogen		244 °C	45
Melting Enthalpy Crystallization	atmosphere according to the ASTM D3418. Heated from 0	DSC	40 J/g	45
temperature	to 270 °C with a rate of 10 °C		165 °C	45
Crystallinity degree	/min		29%	45
glass transition temperature Crystallization	Heated from room temperature		72.9 ± 1.2 °C	46
temperature	to 270 °C with a rate of 10 °C	DSC	$133.5 \pm 0.1 \ ^{\circ}\text{C}$	46
Melting point	/min		$253.4 \pm 0.4$ °C	46
Crystallinity degree			$11.8 \pm 1.8$ %	46
Thermal degradation 5% (N2)	5 mg heated from 23 to 700 °C	TGA	382.3 ± 1.4 °C	46
I hermal degradation 5% (air)	at 10 °C /min		370.1 ± 1 °C	46
Glass transition temperature		DSC	67 °C	47

Crystalli	tion			
tempera	Ire Heated from row	om temperature	208 °C	47
Melting	oint until 300 °C	at 10°C /min	234 °C	47
Melting En	nalpy		38.3 J/g	47
Thermal degra (air)	tion 50% Samples heat	ed from room	428 °C	47
Weight loss Weight percent	420 °C temperature un	til 700 C at 10 To min	GA 14%	47
at 650			0.41%	47

In the research made by Jiang et al. can be noticed thermal differences between virgin and R-PET. They used R-PET obtained from Thailand postconsumer waste bottles, and it was blended with PBAT and Wollastonite. From this investigation was recovered *Figure 6* that shows DSC thermograms of R-PET and V-PET.



*Figure 6.* DSC thermograms of neat recycled (PET-R) and neat virgin PET(PET-V) (Recovered from Kráčalík et al.<sup>48</sup>)

*Figure 6* shows the difference in the thermal transitions of V-PET and R-PET; The Tg of the R-PET is 3.7 °C lower than the V-PET; this difference could be originated in the molecular weight reduction due to the recycling process. After Tg, it is possible to observe a cold crystallization process; this is expected behavior for polyesters, especially for PET. This phenomenon occurs when the sample does not have the necessary time to crystallize during cooling; when the sample is heated above its Tg amorphous PET fraction gain enough energy to move and arrange in a well-organized structure. In this transition, R-PET shows a reduction of 3.2 °C; this reflects the higher mobility of the R-PET chains compared to the V-PET ones. The last signal is the melting process; in this case, there is no difference in the melting point; in general, the changes in the melting point occurs when the degradation is advanced, and the reduction in molecular weight, but not enough to produce changes in the melting temperature.

#### 3.2. PET blendings

In the last section, the thermal and mechanical properties changes after the recycling of PET were evident. During the use of PET, it is known that it is contaminated with some chemicals that can reduce the load capacity of the recycled products, induce fracture, decrease their molar mass and viscosity, and limit the use of R-PET <sup>49</sup>. That is why the blending of polymers during extrusion has been accepted and studied as a tool to produce new materials with properties similar to V-PET or better <sup>50</sup>.

When R-PET is blended with other polymers, two main trends are observed:

- Increase Hardness. This option involves the blending of R-PET with a more rigid material, increase the PET crystallinity, or both.
- Reduce Hardness. This trend focuses on adding a second material with plasticizing properties, originating a new material with less rigidity than R-PET.

*Table 3* summarized the mechanical properties reported for the blends of R-PET. It is possible to find these tendencies in this table.

Matrix	Additive	Composition matrix/additive	Property	ISO/ASTM	Test method	Value (unit)	Reference
			Tensile strength			74±3 MPa	6
			Young modulus			1081 MPa	6
	V-PET	50/50	Cristalinity degree	ISO 527-2 type 1B	Tensile testing	28.8 %	6
			Deformation at break point			28.3 ±0.1 %	6
			Deformation			11.6±0.1 %	6
			Storage modulus (30 °C)			1900± 10MPa	51
			Tensile strength	ASTM D638 M-9	Tensile testing	55±5 MPa	51
	P PBT 7	75/25	Young modulus		-	2200 MPa	51
K-PE1			strain at break			375 ± 75 %	51
			Impact strength	ISO 180 standard	Izod impact	$3.75 \pm 0.25 \text{ KJ}/m^2$	51
			Tensile modulus		Tensile testing	3 GPa	52
			Yield strenght	ASIM D638		2.3 GPa	52
	PC	50/50	Impact strength	ASTM D256	Izod impact test	$1.9 \pm 0.1 \text{ KJ}/m^2$	52
			Fracture toughness	ASTM D 5045	Fracture toughness	$2.3\pm0.1~\mathrm{MPa}/m^2$	52

 Table 3. Mechanical properties of representative R-PET blended with several polymers

SEBS (Styrene- ethylene- butadyene- styrene copolymer)	50/50	Tensile strength	ASTM D638 with strain rate of 5 mm/min	Tensile testing	8.63 MPa	50
		Tenside modulus			2494.1± 74.7 MPa	38
PBAT	80/20	strain at break	ISO 527 estándar 10kN at 50 mm/min	Tensile testing	$2.7 \pm 0.1$ %	38
		Tensile strength			44.2 ± 2 MPa	38
		Tensile strength	ASTM D638-10		57.5 ± 3 MPa	39
PEN (poly(ethylene		Elogation at break	crosshead speed of 5 mm/min	Tensile testing	300%	39
2,6-naphthalate)	70/30	Izod impact strength	ISO 180 standard	Izod impact test	$25 \text{ KJ}/m^2$	39
		Elastic modulus	ASTM D638	Tongila tasting	1697 MPa	53
Polypropylene	50/50	Yield stresses	standard	Tensne testing	31.69 MPa	53
(PP)		Charpy Impact strength	ISO 179 standard	Charpy Impact	$10.54 \text{ J/}cm^2$	53
Bio-PFT		Tenside modulus			$820.5\pm30.2~\text{MPa}$	40
(Obtained from		Tensile strength	ISO 527-1:2012		$57.7\pm2.8~\mathrm{MPa}$	40
nautural		Elongation at break		Tensile testing	$10.8 \pm 1.4 \%$	40
sources)	45/55	Charpy Impact strength	ISO 179-1:2010	Charpy Impact	$1.84 \pm 0.38 \text{ KJ}/m^2$	40
Fly ash, red mud, silica fume, sand	35/6/25/16/28	Compressive strength	ASTM C39	Compressive testing	109.62 MPa	54

Polymers with opposite properties to R-PET are typically used to reduce the R-PET rigidity, with a high strain at break and low tensile modulus. When these polymers are used, a decrease in tensile modulus is experienced as the dispersed phase amount is added. *Figure 7* shows Tensile strength in R-PET/PC and R-PET/PBAT samples. As it can be seen, blendings with PBAT reduce their tensile strength which is attributed to the high flexibility and low tensile modulus of the dispersed phase, which causes a reduction in the stiffness of the blends. However, in R-PET/PC blendings a tensile strength increase can be experienced according the amount of PC that is added to the samples; it is due to an increase in the crystallinity degree of R-PET that reduces the chain mobility of polymers because of the presence of a polymer, in this case PC, with hardness properties<sup>40</sup>.



Figure 7. Tensile strength versus second component content, for R-PET/PC and R-PET/PBAT blends (Adapted from Jiang et al. and Negoro et al.<sup>38,52</sup>)

*Figure* 7 shows the main tendencies on tensile strength for the blends based on R-PET. The blends with a more rigid polymer, as PC, tents to increase the tensile strength when the amount of PC increases; that is to say, this material is designed to harden the R-PET. On the other hand, a softer polymer, like PBAT, produces a decrease in tensile strength with the increase of the softer component; in this case, the idea of this blend is to get a material more flexible than PET. Jiang et al.<sup>38</sup> studied the R-PET blended with

poly(butylene adipate-co-terephthalate) (PBAT). *Figure 8* shows the SEM images of the blends.



*Figure 8. Representative SEM micrographs (x1500 magnification) of the (a) R- PET, (b) neat PBAT, (d) R-PET/PBAT blend at 80/20 wt%, (g) d) R-PET/PBAT blend at 50/50 wt% (Adapted from Jiang et al.*<sup>38</sup>)

These images show a continuous phase; that is to say, the polymers are miscible. Also, it is possible to observe an increase in the deformed zone, indicating an increase in the ductility of the blends when the PBAT is increasing. They found decay in tensile modulus was shown, from 2854 MPa at 10 wt% PBAT down to 981 MPa at 50 wt% PBAT, due to the high flexibility of PBAT, which was confirmed later with DSC analysis. However, the strain at break increased from 1.8% to 5% due to an increase in R-PET crystallinity. As already mentioned, the polymer blend is used to obtain a new material with higher performance due to the balance between mechanical resistance and thermal properties. The critical factor for correct blendings is the compatibility and interaction between polymer phases<sup>52</sup>,<sup>53</sup>. Moreover, when R-PET is being extruded in the extrusion cycle at melting temperatures, the polymer can undergo a degradation process through hydrolysis, oxidation, and transesterification reactions. These reactions lead to the cleavage of the chains into smaller ones with acid and hydroxyl ester end groups generating contamination in the material and drastic losses in ductility<sup>6</sup>. These facts can affect thermal properties, presented in Table 4, and show the result of blending R-PET with other polymers.

Matrix	Additive	Composition matrix/additive	Property	ISO/ASTM	Test method	Value (unit)	Reference
			Crystallization temperature	Samples heated from 30		195.8 °C	38
			Melting point	°C to 300 °C at a rate of 10	DSC	245.8 °C	38
			Melting Enthalpy	°C /min under nitrogen	DSC	43.6 J/g	38
			Crystallinity degree	atmosphere		45.40 %	38
			Onset temperature			412 °C	38
			Thermal degradation 50%	None	TGA	445 °C	38
			Endset temperature			467 °C	38
	PEN		Glass transition temperature			87.9 °C	39
	(poly(ethylene	70/30	Melting point	samples were heated from 25°C to 300°C with a	DSC	247.5 °C	39
	2,6-	Melting Enthalpy heating rate of 10°C/m	heating rate of 10°C/min	DSC	29.6 J/g	39	
	naphthalate)		Crystallinity degree	5		7.30%	39
	Polypropylene (PP)	95/5	Melting point	Samples were heated from 50 °C to 300 °C with a speed of 10 °C/min. It was kept above 300 °C for 2 minutes to complete the	DSC	254 °C	55
			Crystallization temperature	melting		$207 \pm 1$ °C	55
			Crystallinity degree			25%	55
	Bio-PET (Obtained	45/55	Glass transition temperature	samples of 6.1 +- 1.2 mg were heated from 30 to	DSC	82.6 ± 0.9 °C	40
	from nautural sources)		Melting point	280 °C with a speed of 10 °C/min		237.9 ± 1 °C	40
	5041005)		Crystallization temperature	C/IIIII		191.2 ± 0.3 °C	40

Table 4. Thermal properties of representative R-PET blended with several polymers

		Crystallinity degree			$37.0 \pm 0.7$ %	40
		Thermal degradation 5% (air) 5-7 mg heated from 30- 700 °C Speed 20 °C/min		TGA	$393 \pm 0.2$ °C	40
		Residual mass at 700 °C (air)	700 0. Speed 20 C/IIIII		$2.18 \pm 0.05$ %	40
		Melting point	Less 3mg in Al pan heated from room temp. to 200 °C at 10 °C/min	DSC	133 °C	56
PE	50/50	Start degradation temperature	3mg from room		370 °C	56
	20120	End degradation temperature	temperature to 600 °C	TGA	460 °C	56
		Weight loss $f_{2}$ with a flow factor $f_{2}$	10/1	83.60%	56	
		Residue after 500 °C	10°C /min		10.50%	56
		Absoption 7 days			0.105%	54
		Absoption 28 days			0.06%	54
Fly ash red		Absoption 56 days	Specimens sumerged in		0.047 %	54
mud, silica fume_sand	35/6/25/16/28	Weight of specimen before inm.	30% HCl solution for several days	Acid resistance	345.35 g	54
Tunite, Sund		Weight of specimen 7 days			345.17 g	54
		Weight of speciment 21 days			344.71 g	54
		Weight of speciment 28 days			344.05 g	54

The values of the thermal transitions and thermal stability presented in Table 4 are dispersed; there is no clear tendency with the addition of a second phase, the difference in the origin of the R-PET and the nature of the second phase will determine the final properties.

However, the miscibility of a sample could be estimated by determining Tg. When two components are miscible, there is an increasing trend according to the dispersed phase added <sup>57</sup>,<sup>53</sup>. This Tg of the new blend can be predicted using Fox equation to obtain an estimated value for Tg that would be confirmed experimentally. If the result of this experimentations are not close with the Fox prediction, or two Tg are observed, then the blend could be considered inmiscible<sup>58</sup>.

$$\frac{1}{T_g} = \frac{W_1}{T_{g1}} + \frac{W_2}{T_{g2}}$$

Negoro et al.<sup>52</sup>, reported two Tgs for the PC/PET blends; these values were similar to the Tg of each neat polymer, indicating that the blends were immiscible; however, they observed a deviation of Tg with the composition, which indicates a possible interaction between phases.

The presence of two phases was proved employing SEM (see *Figure 9*), in all the figures is possible to observe isolated spheres in a continuous matrix; in the case of *Figure9A* and *B* is possible to observe both spherical particles and holes, indicating a lack of interaction between the phases, however in *Figure 9C* and *D* the spheres was incomplete indicating a stronger interaction between the disperse phase (R-PET) and the matrix (PC)

![](_page_42_Figure_0.jpeg)

*Figure 9. SEM photograpghs of R-PET/PC blends. (A) R-PET/PC (90/10), (B) R- PET/PC (70/30), (C) R- PET/PC (50/50), (D) R-PET/PC (30/70) (Recovered from Negoro et al.*<sup>52</sup>)

As was discussed previously, the blends PET/PBAT are miscible, as was proven with the SEM image (See *Figure 8*), where a continuous phase can be experimented due to good miscibility between PET and PBAT. *Table 5*, shows Tg values for R-PET/PBAT and R-PET/PBAT/Wollastonite samples at different compositions.

*Table 5. Tg* values of *R*-*PET*/*PBAT*/*Wollastonite* samples at different compositios from DSC analysis (Recovered from Jiang et al. )

Samples (R-PET/PBAT/Wollastonite)	Tg (°C)
100/0/0	80.3
90/10/0	68.1
80/20/0	69.6
70/30/0	70.7
60/40/0	92.1
50/50/0	92.1
72/18/10	70.6
64/16/20	73.1
56/14/30	74.0
48/12/40	74.2

Tg of R-PET was 80.3 °C and the inclusion of 10-30 wt% PBAT in R-PET matrix reduced the Tg of the samples by 9.6 to 12.2 °C compared with pure R-PET. This data suggest that low Tg values is due to PBAT (-31 °C) that increased chain mobility of the blends.

However, Tg increased according PBAT compositions increased in the blendings, owing to the increased chain entanglement that restricted the mobility of R-PET and it proves the high miscibility between the components of the samples.

#### 3.3. Chain Extenders and Compatibilizers

A chain extender is a compound with a low molecular weight that is effective even in small quantities and can react with terminal groups of polyesters, interconnect polymer chains, increase molecular weight, and minimize the adverse effect of contaminants<sup>3930</sup>. It is important to notice that chain extenders do not prevent degradation but compensate for its effect on the molar mass of the polymer<sup>30</sup>. Chain extenders can be introduced as an alternative method for improving the miscibility of blendings with transesterification reactions<sup>39</sup>. It rejoins polymer chain segments, compensates the molar mass reduction due to degradation <sup>30</sup>. Modifying the miscibility of blends and increasing molecular weight can provide new mechanical properties summarized in *Table 5* This table shows data collected from Tensile, Flexural, Compressive testing, and Charpy Impact of blending with chain extenders.

Matrix	Additive	Composition matrix/additive	Property	ISO/ASTM	Test method	Value (unit)	Reference
			Tensile strength	ASTM D-638 at cross- head speed of 20	Tensile testing	51 MPa	34
	<b>A</b>		Tensile modulus	mm/min	8	3.4 GPa	34
	Ammonium polyphosphate, Talc	93/2/5	Flexural strength	ASTM D-790 with span length of 48mm and testing speed of	Flexural test	81 MPa	34
			Flexural modulus	3mm/min		3.1 GPa	34
			Tensile strength			$55 \pm 5$ MPa	3
	Polycarbonate, Joncryl ADR4370	68/30/2	Elongation	ASTM-D-638-02	Tensile testing	45 ± 5 %	3
			Tensile Modulus			$2100\pm50~\text{MPa}$	3
R-PET	Joncryl ADR 4300,	06 5/1/2 5	Impact resistance	ASTM D638-10	Tensile testing	14.6 KJ/ $m^2$	37
	Lotader AX8900	90.5/1/2.5	Toughness	ASTW D056-10	Tensne testing	13.1 $MJ/m^3$	37
			Tenside modulus			5576.7 ± 69 Mpa	38
	PBAT, Wollastonite	48/12/40	strain at break	at 50 mm/min	Tensile testing	1.7±0.1 %	38
			Tensile strength			$46.6 \pm 2.1$ MPa	38
	Delemented en e (DD)		Elastic modulus		T'1. 44'	1753 MPa	53
	PP-g-MA (Maleic		Yield stresses	AS1M D038 standard	i ensile testing	31.91 MPa	53
	anhydride)	50/48/2	Charpy Impact strength	ISO 179 standard	Charpy Impact	10.98 J/cm <sup>2</sup>	53

 Table 6. Mechanical properties of representative R-PET blended with several polymers and chain extenders

According to *Table 6*, the tensile strength values for these studies were more or less similar; in this case, this value was around 50 MPa. However, the tensile module was affected by the nature of the other components in the blend. The Young's module is less sensitive to the molecular weight and the interaction between the components; however, the nature of the components highly affects the value. The property that should be more influenced by the interaction between the phases and the molecular weight is the strain at break. However, there is not enough published data to confirm this as a general trend for R-PET blends.

The influence of the chain extenders in the breaking point was demonstrated by Srithep et al.<sup>3</sup>, who used 1% and 2% of chain extender (Joncryl ADR 4370) in R-PET/PC blends with a ratio of 70/30 wt%, respectively. R-PET at the starting point registered a tensile strength value of 10 MPa and, with the addition of 30 wt% PC, it value increased to 17 MPa. These values increased to 39 and 55 MPa for 1% and 2% of chain extender, representing, in contrast with initial blend value, an increase of 229,41% and 323,52%, respectively.

On the other hand, Jiang et al.<sup>38</sup> used Wollastonite as the third component in a blend of R-PET/PBAT to improve the mechanical properties. This improvement was related to the large aspect ratio of Wollastonite which tended to orient in the machine direction during the molding process. For ratios between 0 and 30% by weight, as shown in *Figure 10* by SEM, the Wollastonite dispersed to provide a large contact area that incurred good adhesion of the dispersed phase and the matrix, then the Wollastonite acts as a compatibilizaer in these blends However, for amounts greater than 30% by weight of Wollastonite, the tensile strength decreased due to agglomeration of Wollastonite.

![](_page_46_Figure_0.jpeg)

*Figure 10.* SEM micrographs (x1500 magnification) of the 80/20 wt% R-PET/PBAT blend composites filled with wollastonite at (a) 0 wt%, (b) 10 wt%, (c) 20 wt%, (d) 30 wt%, (e) 40 wt% (Adapted from Jiang et al.<sup>38</sup>)

It is concluded that the rigid particles of Wollastonite restricted the molecular movement of the matrix. However, at higher contents of Wollastonite, the melting flow index increased gradually due to the agglomeration of particles that led to a smaller contact area and facilitated the movement of the polymer chain. Also, Wollastonite induced a carbon residue at high temperature of the compounds, which indicates higher thermal stability of the compounds<sup>59,60</sup>.

*Table 7* shows thermal properties of blendings with chain extenders such as Joncryl ADR4370, among others; and the values obtained from different research experiments at different conditions.

Matrix	Additive	Composition matrix/additive	Property	ISO/ASTM	Test method	Value (unit)	Reference
			Specific viscosity	tateschlaresthans and shanal (the		0.365	61
			Intrinsic viscosity	mass ratio was 1:1) at 25 °C using	Dynamic frecuency	0.655	61
	2, 4, 6, 8-tetra (2, 3-	22.4	Viscosity-average molecular weight	Ubbelodhe viscometer		18310	61
	epoxypropoxy) propane	99/1	Glass transition temperature	tests were made at 280 °C at a constant strain amplitude (10% strain) under a nitrogen gas purge	Dynamic mechanical analysis	106 ℃	61
			Glass transition temperature	Specimens of 4 to 5 mg were		88.9 °C	3
		68/30/2	Melting point	placed in aluminium sample pans and heated from -10°C to 280°C	DSC	224.1 °C	3
R-PET	Polycarbonate,		Melting Enthalpy		250	17.4 J/g	3
	Joncryl		Cristalinity degree			21.3 %	3
	ADK+370		Thermal degradation 10%		Thermal	404.1 °C	3
			Thermal degradation 20%	None	temperature	432.9 °С	3
			Glass transition temperature			68.94 °C	37
Joncryl ADR		Melting point	Heating from 25°C to 300 °C at a	Dac	255.47 °C	37	
	4300, Lotader AX8900	96.5/1/2.5	cristalization temperature	rate of 5 °C/min	DSC	116.33 °C	37
			Melting Enthalpy			49.24 J/g	37
			Cristalinity degree			100%	37

## Table 7. Thermal properties of representative R-PET blended with several polymers and chain extenders

		Melt flow index	ASTM D1238	MFI	87.8 ± 6.3 mm /10min	38
		Crystallization temperature			198.4 °C	38
		Melting point	Samples heated from 30 °C to 300	DSC	245.4 °C	38
PBAT, Wollastonite	PBAT, 48/12/40	Melting Enthalpy	°C at a rate of 10 °C/min under		17.3 J/g	38
wonustonite		Cristalinity degree	mu og en uniosphere		30%	38
		Onset temperature			416 °C	38
	Thermal degradation 50%	None	TGA	480 °C	38	
		Endset temperature			473 °C	38

\_\_\_\_

During degradation of PET, some carboxyl groups are generated, which can be confirmed by FTIR spectra<sup>61</sup>. Wang et al.<sup>62</sup>, used 2, 4, 6, 8-tetra (2, 3-epoxypropoxy) propane as chain extender and was blended with different amounts of chain extender; 0.1%, 0.5%, 1.0%, and 2.0% by weight and such a way samples were reported as PET-0, PET-1, PET-2, PET-3 and PET-4. This research showed, in *Figure 11*, vibrancies at 1340 and 1410  $cm^{-1}$  for PET-4 which peaks are characteristics for -OH of ending carboxyl groups and, were lower than PET-0. A vibration at 1240  $cm^{-1}$  of PET-0 is observed and is assigned to bending vibration of end -OH groups became stronger and two shoulder peaks at 1 260 and 1 280 cm-1 were observed.

![](_page_49_Figure_1.jpeg)

*Figure 11.* FTIR absorption spectra of unmodified PET-0 and highly modified PET-4 normalized on the peak of C=O stretching vibration (1720  $cm^{-1}$ ) (Recovered from Wang et al. <sup>62</sup>)

The presence of these end groups can undoubtedly modify the thermal properties of the blends. Such is the case of the research reported by Jian et al. <sup>38</sup>, who used various blending compositions of R-PET/PBAT and whose results showed a reduction in Tg between approximately 9.6–12.2 °C. The presence of Wollastonite increases Tg in 3.5 °C compared to the initial blending of 80/20 wt% R-PET/PBAT. This increase is due Wollastonite addition in the blending. However, it is important to note that the addition of a chain extender does not ensure the improvement of the mechanical nor thermal properties of the blends. Such is the case reported by Karsli et al.<sup>37</sup> who used Joncryl and Lotader as components shown in *Table8*.

*Table 8.* Compounding of components and code names of products (Recovered from Karsli et al.<sup>37</sup>)

R-PET/Joncryl/Lotader	R-PET (wt%)	Joncryl (wt%)	Lotader (wt%)
R-PET	100	0	0
R-PET_1J	99	1	0
R-PET 1J 2.5L	96.5	1	2.5
R-PET_1J_5L	94	1	5

They reported that the presence of Joncryl and Lotader either separately or together does not contribute to the increase in the glass transition temperature or in the other properties, but on the contrary, it decreased the crystallinity of R-PET as shown in *Table 9*.

Sample code	$T_g(^{\circ}\mathrm{C})$	$T_c$ (°C)	$T_m(^{\circ}C)$	∆H(J/g)	Xc (%)
R-PET	68.94	116.33	255.47	49.24	100
R-PET_1J	68.43	117.76	256.03	45.78	93.91
R-PET_1J_2.5L	68.43	117.89	253.41	47.74	100.47
R-PET_1J_5L	68.94	113.87	254.50	41.61	89.90

*Table 9.* DSC analysis results of samples reported by Karsli et al.37 (Recovered from Karsli et al.<sup>37</sup>)

This result is based on the chain entanglement of R-PET and it is due to the high degree of branching which may resulted from high amount of Lotader impact modifier.

#### 3.4. Filler Nano-particles

The introduction of organic and inorganic nanofillers in polymeric matrices provides the opportunity to improve the mechanical and thermal properties of the polymer matrix. These nanoparticles are characterized by having a large aspect ratio (between 100 to 1500) and a large surface area (between 750 and 800  $m^2/g$ )<sup>42</sup>. Nanofillers provide the polymeric matrix with mechanical resistance, optical clarity, electrical, thermal, chemical, and UV resistance, gas barrier properties, and dimensional stability<sup>42,47</sup> like the table presented below. *Table 10* can be shown how filler nanoparticles can change thermal properties depending on the additive is being blended.

Matrix	Additive	Composition matrix/additive	Property	ISO/ASTM	Test method	Value (unit)	Reference
			Glass transition temperature	Samples in a nitrogen atmosphere heated from 20 to		78.41 °C	42
			Crystallization temperature		DSC	206.61 °C	42
			Melting point	350 °C with a speed of 10 °C /min	DSC	245.29 °C	42
			Melting Enthalpy	/11111		8.19 kJ/kg	42
Cloisite 10A PET Cloisite 15A	95/5	Crystallinity degree			0.94%	42	
			Decomposition temperature	samples heated up to 900 °C under $N_2$ ) flow with a speed of 10 °C/min	TGA	436.12 °C	42
			Thermal degradation 5% $(N_2)$			402.06 °C	42
			Thermal degradation 50% $(N_2))$			447.10 °C	42
			Glass transition temperature	Samples in a nitrogen	DSC	82.70 °C	42
			Crystallization temperature	atmosphere heated from 20 °C		208.66 °C	42
	Cloisite 15A	95/5	Melting point	to 350 °C with a speed of 10		242.62 °C	42
			Melting Enthalpy	C/mm		4.24 kJ/kg	42
			Crystallinity degree			2.51%	42
			Decomposition temperature		TGA	398.12 °С	42

Table 10. Thermal properties of representative R-PET blended with several filler nanoparticles

		Thermal degradation 5% $(N_2)$	samples heated up to 900 °C under $N_2$ flow with a speed of		423.17 °C	42
		Thermal degradation 50% $(N_2)$	10 °C/min			42
		Glass transition temperature	Heated from room		74 °C	47
		Crystallization temperature	temperature until 300 °C at	DSC	203 °C	47
		Melting point	10°C/min		238 °C	47
Cloisite 15A	93/7	Melting Enthalpy			39.1 J/g	47
		Thermal degradation 50%	Samples heated from room	TGA	432°C	47
		Weight loss at 420 °C	temperature until 700 °C at 10		16.10%	47
		Weight percentage residue at 650 °C	°C/min		4.10%	47
		Glass transition temperature			76.28 °C	42
	Crystallizati Melti Melting	Crystallization temperature	Samples in a nitrogen atmosphere heated from 20 °C to 350 °C with a speed of 10 °C/min		209 °C	42
		Melting point		DSC	245.41 °C	42
		Melting Enthalpy			1.95 kJ/kg	42
Cloisite 20A	95/5	Crystallinity degree			0.44%	42
		Decomposition temperature			388.59 °С	42
		Thermal degradation 5% $(N_2)$	samples heated up to 900 °C under $N_2$ flow with a speed of	TGA	408.89 °C	42
		Thermal degradation 50% $(N_2)$	10 °C/min		635.51 °C	42
Cloisite 30B	Ploisite 30B 95/5	Glass transition temperature	Samples in a nitrogen	DSC	77.09 °C	42
_ 1010100 0 0 02		Crystallization temperature	atmosphere heated from 20 to	000	207.63 °C	42

		Melting point	350 °C with a speed of 10		246.19 °C	42
		Melting Enthalpy	°C/min		1.59 kJ/kg	42
		Crystallinity degree			1.57%	42
		Decomposition temperature	samples heated up to 900 °C under $N_2$ flow with a speed of	TGA	388.46 °C	42
		Thermal degradation 5% $(N_2)$			395.34 °C	42
	Thermal degradation 50% $(N_2)$	10 °C/min		444.24 °C	42	
	glass transition temperature			73.8 ± 0.1 °C	46	
		Crystallization temperature	Heated from room temperature to 270 °C with a rate of 10 °C/min 5 mg heated from 23 to 700 °C at 10 °C/min	DSC	119.1 ± 0.5 °C	46
		Melting point			253.5 ± 1.7 °C	46
Graphite	90/10	Crystallinity degree			$15.8 \pm 2 \%$	46
		Thermal degradation 5% $(N_2)$		TGA	386.7±3 °C	46
		Thermal degradation 5% (air)			372.7 ± 2.6 °C	46

These compounds enhance the mechanical interlocking and bridging effects within the components to interrupt crack propagation, taking into account the amount of nanofillers added. <sup>42</sup>. Despite all the benefits that these compounds present, preferably clays, layered silicates must be taken into account due to their hydrophilic nature. As a result, these nanofillers are less compatible with the PET matrix, generating weak chemical interactions between the clay and the polymer<sup>47</sup>.

These nanofillers increased the maximum achievable stretch ratio, leading to a higher molecular orientation and chain extension, subsequently increasing the tensile modulus and tensile strength. On the other hand, thermal stability is also improved since nanocomposites hinder the diffusion of volatiles particles and help carbon formation after thermal decomposition. This slowdown is due to the labyrinth effect of the silicate layers. In the research developed by Kiliç et al.<sup>42</sup> different nanocalys types (Cloisite 10A, Cloisite 15A, Cloisite 20A, Cloisite 30B) were added in R-PET matrices, and their properties were analyzed. From the DSC analysis, as shown in *Figure 12*, the addition of nanoclays decreased the Tg between 1-3 °C for the samples with Cloisite 10A, Cloisite 15A. On the other hand, the melting temperature increased in a range of 1-5 °C while the cold crystallization temperature decreased 1-5 °C<sup>42</sup>.

![](_page_55_Figure_0.jpeg)

*Figure 12.* DSC curves of *R*-PET and clay based *R*-PET nanocomposite samples (Recovered from Kiliç et  $al.^{42}$ )

TGA thermogram analysis was also performed and summarized in *Table 11*. Results showed that the loss of mass increased in the nanocomposites containing organoclay except for the compounds with Cloisite 10A and 20A. Also, it was found that the decomposition temperature is higher in the blend with Cloisite 10A in contrast with Cloisite 30B, a phenomenon associated with greater water retention in Cloisite 30B. Therefore, as the dispersion of the organic clay layers increases, the thermal properties of the samples change and the decomposition temperatures decrease and the mass loss increases<sup>42</sup>.

Sample	T <sub>d onset</sub> (°C)	Remaining (wt%)	5% Mass loss (°C )	50% Mass loss (°C )
rPET1 <sup>a</sup>	375.35	39.97	311.39	355.34
rPET1 <sup>b</sup>	478.46			
rPET1 + $10A^a$	436.12	24.4	402.06	447.10
$rPET1 + 10A^{b}$	466.55			
rPET1 + 15A	398.12	70.6	423.17	
rPET1 + 20A	388.59	49.2	408.89	635.51
$rPET1 + 30B^a$	388.46	1.6	395.34	444.24
$rPET1 + 30B^{b}$	409.53			

**Table 11**. Thermogravimetric decomposition characteristics of R-PET and clay based R-PETnanocomposite samples (Recovered from Kiliç et al.  $^{42}$ )

a First degradation

b Secondary degradation

On the other hand, and like it was discussed and the beginning of the present section. Filler nano-particles modify mechanical properties. This variation is presented in *Table 12*, where can be seen changes in mechanical properties according to the amount and type of filler nanoparticle is being blended.

Matrix	Additive	Composition matrix/additive	Property	ISO/ASTM	Test method	Value (unit)	Reference
			Tensile Modulus			2800 MPa	63
		99/1 %wt	Yield Strength			30 MPa	63
			Strain at yield			5%	63
			Tensile Modulus			3000 MPa	63
	Cloisite 25 A	99/3 %wt	Yield Strength	ASTM D638	Tensile testing	20 MPa	63
			Strain at yield			3%	63
			Tensile Modulus			3600 MPa	63
		99/5 %wt	Yield Strength			40 MPa	63
			Strain at yield			1%	63
<b>R</b> _PET		00/1 Cowt	Young's Modulus			$2.5\pm0.4~\mathrm{GPa}$	64
RILI		<i>33</i> /1 /0wt	Yield Strength			$21.8\pm7.5~\mathrm{MPa}$	64
	Montmorillonite (MMT)	99/3 %wt	Young's Modulus	g's Modulus ASTM D628 Tangila tagtin	Tensile testing	$2.4 \pm \text{GPa}$	64
	wonthormonite (whiti)	<i>5715 1</i> 0 wt	Yield Strength	ASTM D050	Tenshe testing	$35.4\pm13.1~\mathrm{MPa}$	64
		99/5 %wt	Young's Modulus			$2.5\pm0.6~\mathrm{GPa}$	64
		<i>5715 1</i> 0 wt	Yield Strength			Value (unit)         2800 MPa         30 MPa         5%         3000 MPa         20 MPa         3%         3600 MPa         40 MPa         1%         2.5 $\pm$ 0.4 GPa         21.8 $\pm$ 7.5 MPa         2.4 $\pm$ GPa         35.4 $\pm$ 13.1 MPa         2.5 $\pm$ 0.6 GPa         42.0 $\pm$ 10.8 MPa         2.34 cN/dtex         3.52 CV%         42.92%         12.43 CV %         2.43 cN/dtex	64
			Tenacity			2.34 cN/dtex	42
	Cloisite 10 A	95/5 %wt	Tenaerty			3.52 CV%	42
		Breaking elongation ISO 2062 standard Tensile testing	Breaking elongetion	ISO 2062 standard	Tensile testing	42.92%	42
				12.43 CV %	42		
	Cloisite 15 A	95/5 %wt	Tenacity			2.43 cN/dtex	42

## Table 12. Mechanical properties of representative R-PET blended with several filler nanoparticles

					3.94 CV %	42
		Breaking elongation			42.54%	42
		Dreaking clongation		16.06 CV %	42	
		Toposity		2.28 cN/dtex	42	
Cloisite 20 A	95/5 %aut	Tendenty	ISO 2062 standard	Tensile testing	7.55 CV %	42
Cloisite 20 A	9515 <i>I</i> UWI	Breaking elongation			47.58%	42
					16.79 CV %	42
	95/5 %wt	Tenacity			1.98 cN/dtex	42
Cloisite 30 A					9.89 CV %	42
		Breaking elongation			40.07%	42
		Dicaking cioligation			21.68 CV %	42

As shown in *Table 12*, several publications are studying the characterization and synthesis of R-PET/filler nanoparticles. As expected, the general values differ from one to another. This difference can be due to several causes: differences in the properties of the material, type of organic clay, the clay modification process, the molecular weight of the polymer, production temperature, among others<sup>42,47</sup> However, in most cases, filler nanoparticles did not improve mechanical properties in contrast with V-PET. It could be due to reduced polymer orientation and the increased variation in fiber cross-section from large agglomerates of nanoclays, as the research made by Kiliç et al.<sup>42</sup>. They studied blends of R-PET with different nanoclays (10A, 15A, 20A, 30B), and they determined that organoclay layers act as a stress collector in nanocomposite fibers, and a deterioration in mechanical properties are observed due to weak interfacing between the clay and R-PET matrix.

The use of nanoparticles as a reinforcement is reported by Yang et al.<sup>64</sup>, who studied blends of R-PET with Montmorillonite (MMT), with compositions from 0% to 5% obtained by a co-rotating twin-screw extruder. They reported an increase in stiffness and tensile strength with the incorporation of MMT (see *Figure 13*). This increase is related to the good dispersion that led to an effective interaction of the clay and the polyester.

![](_page_59_Figure_2.jpeg)

Figure 13. Mechanical properties of R-PET/MMT (Recovered from Yang et al.<sup>64</sup>)

Finally, in the present review, several strategies and additives were presented focused on improving the mechanical and thermal properties of R-PET. One of the strategies that

showed the best results was the combination of polymers and chain extenders or compatibilizers, like the research reported by Jiang et al., who mixed PBAT in the R-PET matrix incorporating small amounts of Wollastonite that functioned as a compatibilizer. This blend allowed to increase the tensile strength, tensile strain, degree of crystallinity, and thermal stability, achieving a hardening of the material, high resistance to melt dripping, and increased the char residue of the composites during combustion.

On the other hand, if the main objective of researchers is to promote plasticizing properties in R-PET, adding only PBAT in high amounts plasticizes the material because it has lower mechanical properties than R-PET.

It is important to note that due to lack of information in this regard, future research would be oriented to investigate for the adequate filler nanoparticles under correct operating conditions and suitable composition for the increase of mechanical and thermal properties and its possible compatibility in R-PET blendings.

## Chapter IV

## Conclusions and perspectives

From the reviewed articles it is possible to conclude:

- It is important to notice the amounts of additive added in the R-PET matrix, small amounts may not have a considerable effect on the polymer, but excessive amounts could decrease the properties of R-PET due to poor dispersion of the additive.
- It is necessary to add chain extenders (an increase of molecular weight), compatibilizer agents and/or filler-nanoparticles (an increase of miscibility) to improve the mechanical and thermal properties of R-PET with other polymers.
- Two main strategies are observed when obtaining reinforcements with R-PET. The first is aimed at hardening the material using a dispersed phase with a Young's modulus greater than that of the matrix or, due to the dispersed phase, despite having a stiffness less than or equal to that of the matrix, adheres to the matrix, thus generating a hardening mechanism that can result in an increase in the degree of crystallinity of the mixture due to nucleating effects, such is the case presented by PC contents. The second trend focuses on the addition of a polymer in such a way that it generates plasticizing properties, with less rigidity than recycled PET, like the case with PBAT contents.
- The optimal balance of mechanical properties is achieved using blendings with three main components, including a compatibilizer or a chain extender.
- Future research should focus on the study of clay nanocomposites, as the case presented with MMT, because of insufficient information in this regard and the high interest of industries for plastics reusing.

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